Geochemical modeling of vent fluid-seawater interactions

Image from NOAA-PMEL.

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photo by Pat Hickey.

Mixing of vent fluid and seawater in the subsurface

Mixing of vent fluid and seawater in chimney walls

Mixing of vent fluid and seawater in flanges

Styles of vent fluid-seawater mixing

Photo taken by submersible *Alvin* of white smokers at TAG active hydrothermal mound, G.Thompson/P.Rona Chief Scientists, 1990. Mixing of vent fluid and seawater in diffusers

Styles of vent fluid-seawater mix

In diffusers, relatively high rates of vent fluid flow through very porous (48% to 87% pore space) zones.

 $\overline{2 \text{ mm}}$

Styles of vent fluid-seawater mixing

Le Bris et al., 2005 In diffusers, outer surfaces are often colonized, with fluid flowing outward across communities.

I. Styles and models of mixing between two fluids In crust In deposits at seafloor In plumes Plume

Have just reviewed many of the different styles

I. Styles and models of mixing between two fluids In crustIn deposits at seafloor PlumeIn plumes II. Reasons to quantify mixing styles Estimate environmental $2^{\circ}C$ seawater conditions in inaccessible locations 350° C Calculate available metabolic vent fluid chimney energy

Why quantify mixing styles?

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Will first review the available tools

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cold.

oxvgenated

seawater

diffuse

flow

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VI. Limitations in current ability to quantify processes

Tools available

▶ I. Distribution of species as fn of T (MINEQL, EQ3, REACT) Sensitivity to input

A. thermodynamic data

B. fluid composition data

C. temperature data

II. Path reaction

- A. assumptions about kinetics
- B. assumptions about whether T is conservative
- III. Transport-reaction
	- A. small scale across steep gradients
	- B. large scale at low transport rates
	- C. assumptions kinetics, boundary conditions, steady-state

Distribution of species as function of T, P

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Thermodynamic data: SUPCRT92 (Johnson et al., 1992; additional internally consistent data)

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Use to calculate available energy:

$$
SO_4^2
$$
² + 2H⁺ + 4H₂ \leftrightarrow H₂S + 4H₂O

 $\overline{}$

+

∆G= ∆Gº + 2.303RTlogQ

 $(\Delta \mathsf{G}^\mathsf{o}$ = -2.303RTlogKeq

So when $\Delta {\sf G}$ = 0, K $_{\sf eq}$ =Q)

Q=(aH₂S)/[(aSO₄=)(aH+ $)^{2}$ (aH₂)⁴]

∆G<0, energy is available.

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 \overline{a}

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Q=[(aSO₄⁼)(aH⁺)²]/[(aO₂)² (aH₂S)]

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Use to calculate available energy:

But temperature often NOT conservative. For example in the TAG active mound, Sr isotopes indicate mix >50 to 99% seawater, but fluid inclusion data indicate temperatures of ~350ºC.

Within and around Alvinellid tubes, T – pH best explained by conductive cooling and heating of vent fluid and seawater.

SO_4^2 ⁻ + 2H⁺ + 4H₂ \leftrightarrow H₂S + 4H₂O $H_2S + 2O_2 \leftrightarrow SO_4^{2} + 2H^+$ What if inhibit hydrogen oxidation? H_2 (aq)+0.5O₂(aq) = H_2O

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Shock and Holland, 2004

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In sulfide-rich vent deposits, must consider transport of heat, which, if by diffusion, is much more rapid than transport of mass:

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Because activity coefficients change with T, must consider the gradient in activity coefficients as well as the gradient in concentration of each species

Assumes reaction rates are slow relative to transport (e.g., steady-state gradients are established in hours to at most 1 day; Tivey and McDuff, 1990)

 $Q=[(aSO_4=(aH^+)^2]/[(aO_2)^2(aH_2S)]$

From Tivey, 2004 Note: log activity is important, so minor differences in activity do not greatly affect energy available; pH and T of redox transition have much greater effect.

From Tivey, 2004

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More complicated 1-D and 2-D coupled transport-reaction models that consider conservation of fluid mass in the system:

$$
\frac{\partial \phi}{\partial t} = -\nabla \cdot \mathsf{q}
$$

where ϕ is porosity, q the velocity vector

And conservation of solute mass:

$$
\frac{\partial (\phi C_i)}{\partial t} + \nabla \cdot (J_{\text{disp}} + J_{\text{adv}} + J_{\text{diff}}) = R_i
$$

where C is moles/m 3 fluid, R is net rate (moles i/m 3 rock/s) for all chemical reactions, J is flux (dispersive (disp), diffusive (diff), and advective (adv); Steefel and Lasaga, 1990.

Need information on kinetics of various reactions, on how changes in porosity affect permeability. If fluid flow (advection) is rapid, it is not possible to fully couple the equations.

IV. Best tools for specific environments

Diffuse flow – Mixing using path reaction model

Plumes – Path reaction model with precipitation allowed and hydrogen oxidation inhibited Plume

Chimney walls – Transport through porous/permeable media

V. Sensitivity of results to assumptions made

Is temperature conservative?

Should some reactions be inhibited?

Is mixing a good approximation for question being asked?

Are boundaries really at steady-state?

TC8-4=middle of chimney wall. TC8-1=outside chimney wall

So the temperature, and likely the fluid composition, at the exterior of the deposit varies on ~12 hr time-scale.

Boundary conditions (e.g., T and maybe composition) at chimney exteriors can vary periodically due to tidally driven bottom currents andwafting of warm fluids

BM72

(Pagé et al., submitted)

VI. Limitations in current ability to quantify processes

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Need information on reaction rates.

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For example with diffusers, flow rates are large enough so that transport by diffusion and advection

cannot be calculated.

Key points to remember: Models are tools dependent on quality of input

Can be used very effectively to test significance of various parameters/assumptions change 1 piece of input and run again

- match observed field data

In most vent environments, transport dominates, so reactants are not limiting, and products are carried away Models are best used

coupled to collection of field/laboratory data.