Geochemical modeling of vent fluid-seawater interactions



Image from NOAA-PMEL.

Meg Tivey, Associate Scientist Dept of Marine Chemistry and Geochemistry Woods Hole Oceanographic Institution Woods Hole, MA 02543 Research funded by









Mixing of vent fluid and seawater in the subsurface



Mixing of vent fluid and seawater in chimney walls



Mixing of vent fluid and seawater in flanges

Styles of vent fluid-seawater mixing



Photo taken by submersible *Alvin* of white smokers at TAG active hydrothermal mound, G.Thompson/P.Rona Chief Scientists, 1990. Mixing of vent fluid and seawater in diffusers

Styles of vent fluid-seawater mixing



In diffusers, relatively high rates of vent fluid flow through very porous (48% to 87% pore space) zones.

Styles of vent fluid-seawater mixing







Le Bris et al., 2005 In diffusers, outer surfaces are often colonized, with fluid flowing outward across communities.

2 mm



I. Styles and models of mixing between two fluids In crust In deposits at seafloor In plumes

Have just reviewed many of the different styles



I. Styles and models of mixing between two fluids In crust In deposits at seafloor Plume In plumes II. Reasons to quantify mixing styles Estimate environmental 2°C seawater conditions in inaccessible locations flange 350°C Calculate available metabolic vent fluid chimney energy

2°C seawater

pool 350°C

diffuse

flow

hot, reduced hydrothermal fluid cold.

oxygenated

seawater

Why quantify mixing styles?

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Will first review the available tools



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Tools available

I. Distribution of species as fn of T (MINEQL, EQ3, REACT) Sensitivity to input

A. thermodynamic data

B. fluid composition data

C. temperature data

II. Path reaction

- A. assumptions about kinetics
- B. assumptions about whether T is conservative
- **III.** Transport-reaction
 - A. small scale across steep gradients
 - B. large scale at low transport rates
 - C. assumptions kinetics, boundary conditions, steady-state

Distribution of species as function of T, P

Fluid composition					
	OBS				
	mmol/kg				
Ca ²⁺	15.6				
Mg^{2+}	0				
K^+	23.2				
Na^+	428.5				
Fe^{2+}	1.664				
Mn^{2+}	0.960				
Ba^{2+}	0.008				
Zn^{2+}	0.106				
Pb^{2+}	0.000308				
Cu^+	0.035				
CO_2	6				
CH ₄	0.07				
SO_4^{2-}	0				
$\mathrm{NH_4}^+$					
Cl	489				
HS	7.3				
SiO_2	17.6				
H ₂	1.673				
рН, 25°С	3.4				
<u> </u>	350	4007			
	von Damm et al.	<u>, 1985</u>			

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Thermodynamic data: SUPCRT92 (Johnson et al., 1992; additional internally consistent data)

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pH, in situ	4.3					
T (°C)	350 🗲					
	Von Damm et al., 19	985				

Distribution of species as function of T, P



Thermodynamic data: SUPCRT92 (Johnson et al., 1992; additional internally consistent) Tools available

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Titration process









Titration process





Titration process















Use to calculate available energy:

$$\mathrm{SO_4}^{2-} + 2\mathrm{H}^+ + 4\mathrm{H}_2 \leftrightarrow \mathrm{H}_2\mathrm{S} + 4\mathrm{H}_2\mathrm{O}$$

 $\Delta G = \Delta G^{\circ} + 2.303 RT log Q$

 $(\Delta G^{\circ} = -2.303 RT log Keq$

So when $\Delta G= 0$, Keq=Q)

 $Q=(aH_2S)/[(aSO_4^{=})(aH^{+})^2(aH_2)^4]$

 Δ G<0, energy is available.



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Use to calculate available energy:





But temperature often NOT conservative. For example in the TAG active mound, Sr isotopes indicate mix >50 to 99% seawater, but fluid inclusion data indicate temperatures of ~350°C.





Within and around Alvinellid tubes, T – pH best explained by conductive cooling and heating of vent fluid and seawater.



Le Bris et al., 2005



What if inhibit hydrogen oxidation? $H_2(aq)+0.5O_2(aq) = H_2O$ $=SO_4^{2^2} + 2H^+ + 4H_2 \leftrightarrow H_2S + 4H_2O$ $=H_2S + 2O_2 \leftrightarrow SO_4^{2^2} + 2H^+$



McCollom and Shock, 1997

Temperature (°C)



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Shock and Holland, 2004





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In sulfide-rich vent deposits, must consider transport of heat, which, if by diffusion, is much more rapid than transport of mass:



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Because activity coefficients change with T, must consider the gradient in activity coefficients as well as the gradient in concentration of each species

Assumes reaction rates are slow relative to transport (e.g., steady-state gradients are established in hours to at most 1 day; Tivey and McDuff, 1990)







 $Q=[(aSO_4^{=})(aH^{+})^2]/[(aO_2)^2(aH_2S)]$

Note: log activity is important, so minor differences in activity do not greatly affect energy available; pH and T of redox transition have much greater effect.



From Tivey, 2004



From Tivey, 2004

	Chimney 120°C 2°C 350°C		<u>2°C</u> Flange <u>120°C</u> <u>350°C</u>	
Mixing style	<45°C	45°C to 80°	80°C to 120°C	Note
OBS-SW	рН~6-7 38°С рН~6	pH~6	pH~5.5-6	sensitivities
mix	$\leq -8.0^{80}, \leq -1.9^{M}$	<u> ≤-7.5 ^{sr}</u>	<u> ≤-6.5^M</u>	of results
OBS-SW	pH~3-7 pH<3	pH<3	pH<3	(e g pH and
diff	9°C ≤-7.0 ^{so} ≤-1.6 ^M	 ≤-15.4 ^{SR}	 ≤-9.3 ^M	T of redox transition)
OBS-SW	pH~7-8 21°C pH~6.5-7	pH~4-6.5	pH~3.5-4	to fluid
sw in	≤-0.9 ^{so}	1	1	compositions
	≤-1.0 ^M	$\leq -6.5^{\text{SR}}$	I ≤-4.0 ^M	and transport
OBS-SW	3°C pH~3	PH~6	pH~5.5 to 6	
vf in	≤-13.8 ^{sr} , ≤-10.2 ^m			styles.
OBS	pH~3.4	pH~3.4	pH~3.4	
cond cool		<u> ≤-16.5 [™]</u>		
Grotto-SW	pH~3-8 27 °C pH<3	pH<3	pH<3	
diff	<u>≤-10.7³⁰,≤-11.7^M</u>	<u>≤-3.0^{3K}</u>	<u> </u> ≤-1.5 ^M	
Grotto-SW	pH~7-8	^{pH~4-7}	pH~4 92°C pH~3.5-4	
SW IN	≤ -4.2 , ≤ -8.9		<u>≤-0.7 ° , ≤-0.2 ° </u>	
Grouo-Sw	рн<3-8 рн<3	 	pri<5	Yellow, highly reduced;
¥1 III	<-6.6 ^{so}	<-3.7 ^{SR}	I	orange, relatively oxidized; sulfate reduction SR
	<-7.2 ^M	≤-1.9 ^M	Ì	sulfide oxidation, SO;
Grotto	pH~4.2	pH~4.2	pH~4.2	methanogenesis, M (yellow); methanotrophy, M (orange).
cond cool		<u>≤</u> -3.5 ^M		OBS-SW mix data are from McCollom and Shock [1997].
				From Tivey, 2004

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More complicated 1-D and 2-D coupled transport-reaction models that consider conservation of fluid mass in the system:

where ϕ is porosity, q the velocity vector

And conservation of solute mass:

$$\frac{\partial (\phi C_{\underline{i}})}{\partial t} + \nabla \cdot (J_{disp} + J_{adv} + J_{diff}) = R_{\underline{i}}$$

where C is moles/m³ fluid, R is net rate (moles i/m³ rock/s) for all chemical reactions, J is flux (dispersive (disp), diffusive (diff), and advective (adv); Steefel and Lasaga, 1990.

Need information on kinetics of various reactions, on how changes in porosity affect permeability. If fluid flow (advection) is rapid, it is not possible to fully couple the equations.

IV. Best tools for specific environments

Diffuse flow – Mixing using path reaction model

Plumes – Path reaction model with precipitation allowed and hydrogen oxidation inhibited Plume

Chimney walls – Transport through porous/permeable media



V. Sensitivity of results to assumptions made

Is temperature conservative?

Should some reactions be inhibited?

Is mixing a good approximation for question being asked?

Are boundaries really at steady-state?





TC8-4=middle of chimney wall. TC8-1=outside chimney wall

So the temperature, and likely the fluid composition, at the exterior of the deposit varies on ~12 hr time-scale.

Boundary conditions (e.g., T and maybe composition) at chimney exteriors can vary periodically due to tidally driven bottom currents and wafting of warm fluids



(Pagé et al., submitted)

VI. Limitations in current ability to quantify processes

Models assume steady-state.

Need information on reaction rates.

If flow rates are very high, problems occur, cannot converge on solution.



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For example with diffusers, flow rates are large enough so that transport by diffusion and advection by

cannot be calculated.





Key points to remember: Models are tools dependent on quality of input

Can be used very effectively to test significance of various parameters/assumptions

- change 1 piece of input and run again
- match observed field data

In most vent environments, transport dominates, so reactants are not limiting, and products are carried away



Models are best used coupled to collection of field/laboratory data.